# Theory 2b

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Freeze-Drying in Practice
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# Theory 2b

- Basic principles of freeze drying processes
  - Physical understanding
  - Critical process parameters
- Development and composition of a (biological) formulation
- Development of a lyophilization cycle: Practical advice
  - How to approach it? What are the most important parameters?
  - How to choose them?
  - Development of cycles for practical work





# Development of a lyophilization cycle: Practical advice



## Where to find guidance?

Pretty good starting point:

Pharmaceutical Research, Vol. 21, No. 2, February 2004 (© 2004)

Review

### Design of Freeze-Drying Processes for Pharmaceuticals: Practical Advice

Xiaolin (Charlie) Tang1 and Michael J. Pikal1,2

https://doi.org/10.1023/B:PHAM.0000016234.73023.75

Pharmaceutical Research (2023) 40:2433–2455 https://doi.org/10.1007/s11095-023-03607-9

#### ORIGINAL RESEARCH ARTICLE

Practical Advice on Scientific Design of Freeze-Drying Process: 2023 Update

Serguei Tchessalov<sup>1</sup> · Vito Maglio<sup>1</sup> · Petr Kazarin<sup>2</sup> · Alina Alexeenko<sup>2</sup> · Bakul Bhatnagar<sup>1</sup> · Ekneet Sahni<sup>3</sup> · Evgenyi Shalaev<sup>4</sup>





### How to approach it?

- Identify the maximum allowable/target product temperature during 1° drying
- Process design
  - Determine an adequate freezing procedure (annealing? Controlled nucleation?)
  - Ramps, equilibration steps, target freezing temperature, hold times
- 1°drying (simulation models or "paper-based")
  - Determine combination of chamber pressure and shelf temperature
  - Ramp
  - Drying time (isothermal hold)
  - PAT for endpoint determination
- 2° drying
  - Ramp
  - Target shelf temperature and isothermal hold time





## Freezing – advice for process design

- Decide if thermal treatment (annealing or controlled ice nucleation) shall be implemented → Theory 9
- Define loading temperature (usually: room temperature)
- Define process:
  - Equilibration step: decide temperature (above eq. freezing point) + hold time (min. 30min)
  - Coolin ramp rate  $(0.2 2 \, ^{\circ}\text{C/min}) \rightarrow$  for scalability reasons:  $0.3 0.7 \, ^{\circ}\text{C/min}$
  - Target temperature: min. 5°C below Tg' (in most cases -40 to -45°C will do the job)
  - Hold time dependent on fill depth: ≤ 1cm: 1h, 1-2 cm: 2h, >2h: 4h

Based on: 1) "Practical Advice on Scientific Design of Freeze-Drying Process: 2023 Update." Tchessalov et al. Pharm Res 40, 2433–2455 (2023)., 2) "Design of Freeze-Drying Processes for Pharmaceuticals: Practical Advice". Tang, X., Pikal, M.J. Pharm Res 21, 191–200 (2004).





# Primary Drying – advice for process design I

- Determine the target product temperature (T<sub>D</sub>): amorphous formulations
  - For drying times >2d:  $T_{collapse}/T_{eutectic}$  minus 2°C
  - For drying times <10h: T<sub>collapse</sub> minus 5°C
  - For drying times  $10 \le t \le 2d$ : T<sub>collapse</sub> minus 3°C
  - Safety margin can also be calculated\*
  - For (semi-)crystalline products: depending on equipment capabilities, a  $T_p$  of ~-10°C to -15°C is recommended (dependent on  $T_{eu}$  of the crystalline solute)
- Next, either use a simple heat/mass transfer model like 1) SP Scientific LyoCalculator or 2) LyoPRONTO or determine  $\mathbf{p}_{chamber}$  and  $\mathbf{T}_{shelf}$  "by hand"
- Ramp rate typically: 0.5 1 °C/min

<sup>\*&</sup>quot;Impact of natural variations in freeze-drying parameters on product temperature history: application of quasi steady-state heat and mass transfer and simple statistics." Pikal et al. AAPS PharmSciTech. 2018;19(7):2828–42.





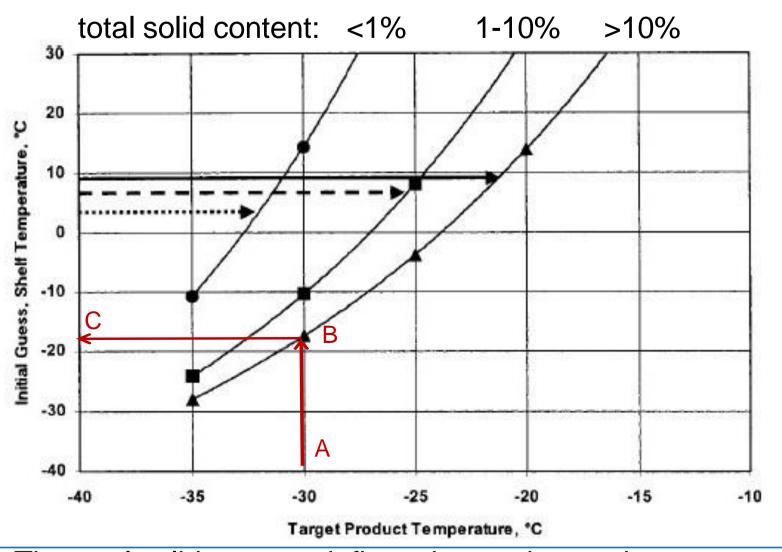
### Side note: Online calculators (heat/mass transfer simulations)

- SP Scientific LyoCalculator (based on Pikal et al. model)
  - Not officially available anymore, but still can be accessed <u>here:</u>
  - <a href="http://web.archive.org/web/20200924004836/http:/www.spscientific.com/LyoCal">http://web.archive.org/web/20200924004836/http://www.spscientific.com/LyoCal</a> c/Lyocalculator.html
- LyoPRONTO (Shivkumar et al.)
  - Open source, theoretical assumptions in journal article
  - <u>Tutorial</u> available as book chapter
  - extended features like freezing calc, primary drying calc, design space calc, primary drying optimizer, but needs more advanced knowledge
  - Can be accessed here: <a href="https://lyopronto.geddes.rcac.purdue.edu/">https://lyopronto.geddes.rcac.purdue.edu/</a>





# Primary Drying – shelf temperature estimation



Initial shelf temperature estimation:

$$T_c = -27^{\circ}C$$



 $T_p$  2-3°C below of  $T_c$  $\rightarrow$  For instance  $T_p$  = -30°C [A]



Setting of T(shelf) depends on product resistance and thus on total solid content (sc); Example: 11% solid content [B]



Readout is shelf temperature setpoint on y-axis: ~ -18 °C [C]

The total solid content defines the product resistance.

Reprinted from "Design of Freeze-Drying Processes for Pharmaceuticals: Practical Advice". Tang, X., Pikal, M.J. Pharm Res 21, 191–200 (2004). Copyright [2004] © Springer Nature.



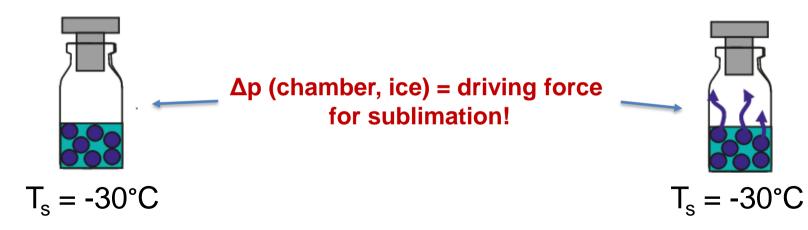
# Primary Drying - Chamber pressure (p<sub>c</sub>) estimation

Chamber pressure > Vapor pressure of ice at sublimation interface

Chamber pressure < Vapor pressure of ice at sublimation interface

p<sub>c</sub>: 500 mTorr (0.67 mbar)

p<sub>c</sub>: 100 mTorr (0.13 mbar)



- Vapor pressure of ice at -30°C → 0.31 mbar = 290 mTorr
- Empiric equation:  $P_c = 0.29 \cdot 10^{(0.019 \cdot T_p)}$

 $p_c$  given in [Torr];  $T_p$  = target product temp.

• For instance:  $\mathbf{p_c}$  (Torr) = 0.29\*10^(0.019\*(-30)) = 0.078 Torr = **78 mTorr** 





## Vapor pressure of ice

Source: https://www.lyotechnology.com/assets/vpoi-chart-101915.pdf

#### Vapor Pressure of Ice

In contact with its own vapor

Temp	Va	por Pressu	ıre	Temp	Va	por Pressu	ıre
°C	Pa	µmHg	μbar	°C	Pa	μmHg	μbar
0	611.1	4584.4	6111	-42	10.22	76.6	102
-2	517.7	3883.6	5177	-44	8.10	60.8	81
-4	437.4	3281.6	4374	-46	6.39	48.0	64
-6	368.7	2765.9	3687	-48	5.03	37.7	50
-8	309.9	2325.1	3099	-50	3.94	29.5	39
-10	259.9	1949.4	2599	-52	3.07	23.0	31
-12	217.3	1630.0	2173	-54	2.38	17.9	24
-14	181.2	1359.1	1812	-56	1.84	13.8	18
-16	150.6	1130.1	1506	-58	1.41	10.6	14
-18	124.9	936.9	1249	-60	1.08	8.1	11
-20	103.2	774.4	1032	-62	0.82	6.2	8.2
-22	85.07	638.2	851	-64	0.62	4.7	6.2
-24	69.88	524.3	699	-66	0.47	3.5	4.7
-26	57.23	429.3	572	-68	0.35	2.6	3.5
-28	46.71	350.4	467	-70	0.26	2.0	2.6
-30	38.00	285.1	380	-72	0.19	1.5	1.9
-32	30.81	231.1	308	-74	0.14	1.1	1.4
-34	24.89	186.7	249	-76	0.10	0.8	1.0
-36	20.03	150.3	200	-78	0.08	0.6	0.8
-38	16.07	120.5	161	-80	0.05	0.4	0.5
-40	12.84	96.3	128	-82	0.04	0.3	0.4

mbar = 750.1 microns

1 micron = 0.1333 Pa

1 Pa = 7.5006 microns

1 mbar = 100 Pa

1 micron = 0.0013 mbar

1 Pa = 0.01 mbar

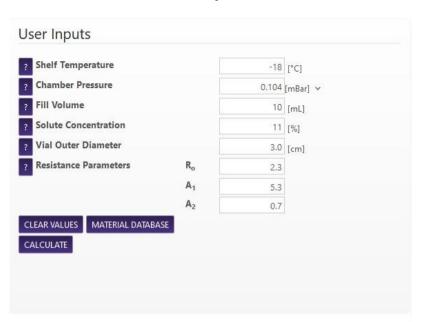
mbar (cgs units) = millibar (10 E3 dyns/cm sq) microns = micrometers of mercury Pa (SI units) = Pascals (N/m²) micron = µmHg = mTorr





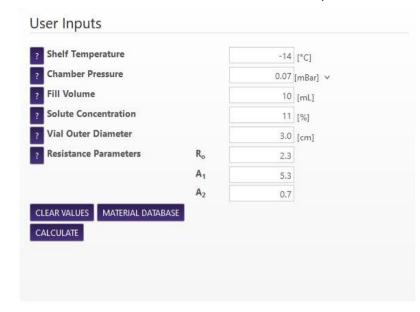
Simulations (assuming: 20R vial, 10 mL fill, 11% total solid content, Tp=-30°C, amorphous)

Simulations for "by hand" estimates:



 $Ts = -18 \, ^{\circ}C$  $p_c = 0.1 \text{ mbar}$ 

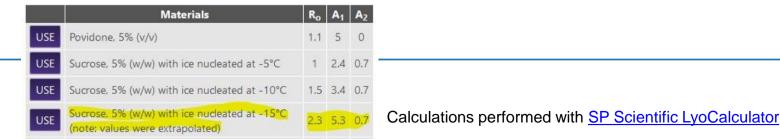
### Simulations optimizing for $T_p = -30$ °C:

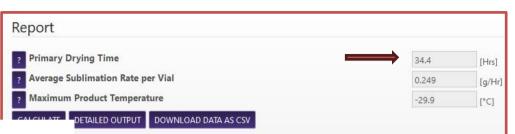


 $Ts = -14 \, ^{\circ}C$  $p_{c} = 0.07 \text{ mbar}$ 



Material Database







# Secondary drying - advice for process design

- Define ramp and target shelf temperature; p<sub>c</sub> not too important\*
- Ramp is critical for preventing collapse (amorphous products)
  - 0.1 to 0.2 °C/min amorphous
  - 0.3 to 0.4 °C/min (semi-)crystalline
- Define isothermal hold at target shelf temperature
  - Often, 3-6h at 40-50 °C suffice to reach < 0.5% (w/w) RMC (see theory 2a, slide 19 for sucrose 5-15%)</li>

<sup>\*</sup> Pc has almost no impact on drying rate, if kept below 0.267 mbar; for further details refer to: "The secondary drying stage of freeze drying: drying kinetics as a function of temperature and chamber pressure". Pikal et al. Int. J. Pharm. 60:3 (1990),







# Development of cycles for practical work





# Experimental overview

- 3 different lab freeze dryers are available for runs
- Five different model formulations will be prepared and freeze dried: Composition of formulations

#	Formulation	BSA	Excipient	Solid content	Buffer system	Surfactant	Ĩ <sup>6</sup> , \ Ĭ <sup>6ñ</sup>	Fill volume
1	Formulation 1	25 mg/mL	240 mM Sucrose	~105 mg/mL			~ -27	10 mL
2	Formulation 2/3	_	240 mM	~80 mg/mL	20 mM	0.02%	~ -32	10 mL
3			Sucrose		HisHCl pH	(w/v)		5 mL
4	Formulation 4	-	120 mM Sucrose	~40 mg/mL	6.0	Polysorbat 20	~ -32	10 mL
5	Formulation 5	-	220 mM Mannitol	~40 mg/mL			~-1	10 mL

• Suggestion: run three differently conservative/aggressive cycles to observe different process behaviors and product appearance





# Available freeze dryer equipment

PAT	Epsilon 2-6D Lyo I	Epsilon 2-6D Lyo II	Epsilon2-4 Lyo III
Pirani	X	X	X
MKS	X	X	-
Comparative pressure measurement	XX	XX	-
PT100 (TC)			
WTM+ (wireless TC)	X	X	X
LyoRx	X	X	X
LyoCam	X	X	X
Controlled nucleation	X	-	-
Mass spectrometry	-	X	-
$\Delta T_p/\Delta T_s$	X	X	-





# working sheet **Conservative**

### **Lyophilization Program**

<u>Product assumptions</u>:  $T_g' = -32$  °C; drying safely **below**  $T_g'$ ; 8% solute conc.

Regulation of vacuum: x Pirani 

MKS Target T<sub>p</sub> = -34 °C

_									<u> </u>			
	Process step	Manual mode: Loading (Pre-cooling)	Freezing	Freezing	Freezing	Freezing	1° drying	1° drying	1° drying	2° drying	2° drying	Manual mode: stooper ing
	Time (hh:mm)		0:15	01:00	0:45	02:00	00:01	00:20	52:00	05:50	02:00	
	Shelf temp. (°C)	20	5	5	-40	-40	-40	-20	-20	50	50	
	Vacuum (mbar)	off	off	off	off	off	0.12	0.12	0.12	0.12	0.12	750
	Safety pressure (mbar)	off	off	off	off	off	0.26	0.26	0.26	0.26	0.26	
	Δ T shelf (°C)		off	off	off	off	off	off	off	off	off	
	Δ T product (°C)		off	off	off	off	off	off		off	off	
	LyoControl Rx (%)		off	off	off	off	off	off	off	off	off	
	camera interval (min)		15	60	1	5	10	10	10	10	60	

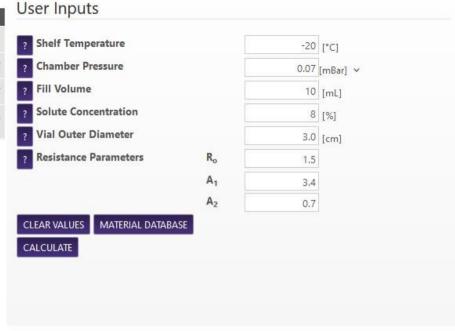




# Conservative Cycle

### Material Database

	Materials	Ro	A <sub>1</sub>	A <sub>2</sub>	
USE	Povidone, 5% (v/v)	1.1	5	0	
USE	Sucrose, 5% (w/w) with ice nucleated at -5°C	1	2.4	0.7	
USE	Sucrose, 5% (w/w) with ice nucleated at -10°C	1.5	3.4	0.7	
USE	Sucrose, 5% (w/w) with ice nucleated at -15°C (note: values were extrapolated)	2.3	5.3	0.7	



Drivery Draine Time	1022	
Primary Drying Time	40.9	[Hrs]
Average Sublimation Rate per Vial	0.218	[g/Hr]
Maximum Product Temperature	-34,0	[°C]

#### Calculated "by hand":

- $T_s = -21 \, ^{\circ}C$
- $Pc = ~66 \text{ mTorr} = 88 \mu \text{bar}$



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working sheet **Regular** 

### **Lyophilization Program**

<u>Product assumptions</u>:  $T_c = -30^{\circ}C$ ; drying around/slightly above  $T_c$ ;

Regulation of vacuum: □Pirani x MKS 8% solute conc.; Target T<sub>p</sub> = -30 °C

Implement Annealing?	Process step	Manual mode: Loading (Pre-cooling)	Freezing	Freezing	Freezing	Freezing	1° drying	1° drying	1° drying	2° drying		Manual mode: stooper ing	
$T_s = -15^{\circ}C$ 3h hold	Time (hh:mm)		0:15	01:00	0:45	02:00	00:01	00:26	32:00	05:20	02:00		
Additional	Shelf temp. (°C)	20	5	5	-40	-40	-40	-14	-14	50	50		
time: 25+180+25	Vacuum (mbar)	off	off	off	off	off	0.07	0.07	0.07	0.07	0.07	750	
+120 = 5h 50m	Safety pressure (mbar)	off	off	off	off	off	0.26	0.26	0.26	0.26	0.26		
	Δ T shelf (°C)		off	off	off	off	off	off	off	off	off		
	Δ T product (°C)		off	off	off	off	off	off		off	off		
	LyoControl Rx (%)		off	off	off	off	off	off	off	off	off	-	
	camera interval (min)		15	60	1	5	10	10	10	10	60		



# Regular Cycle

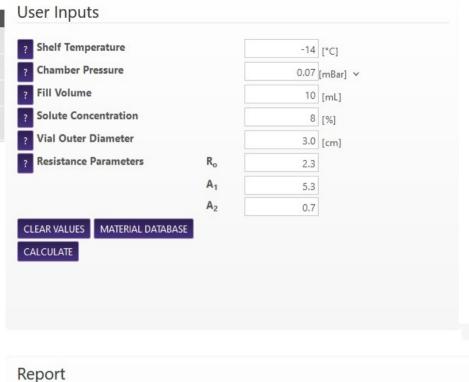
? Primary Drying Time

Average Sublimation Rate per Vial Maximum Product Temperature

CALCULATE DETAILED OUTPUT DOWNLOAD DATA AS CSV

#### Material Database

	Materials	Ro	A <sub>1</sub>	A <sub>2</sub>
USE	Povidone, 5% (v/v)	1.1	5	0
USE	Sucrose, 5% (w/w) with ice nucleated at -5°C	-1	2.4	0.7
USE	Sucrose, 5% (w/w) with ice nucleated at -10°C	1.5	3.4	0.7
USE	Sucrose, 5% (w/w) with ice nucleated at -15°C (note: values were extrapolated)	2.3	5.3	0.7



2.2.2.0	
35.9	[Hrs]

[°C]

#### Calculated "by hand":

- $T_s = -10 \text{ to } -15 \,^{\circ}\text{C}$
- $Pc = ~78 \text{ mTorr} = 104 \mu bar$





working sheet

### Lyophilization Program

<u>Product assumptions</u>:  $T_g' = -27^{\circ}C$ ; drying above T<sub>q</sub>'; 10.5% solute conc.

Target  $T_p = -25$  to -26°C

Regulation of vacuum: □Pirani xMKS

	Aggressive	
Implement CN here? LyoCalc w/ -5° Suc	Process step	
	Time (hh:mm)	
	Shelf temp. (°C)	
	Vacuum (mbar)	
	Safety pressure (mbar)	
	Δ T shelf (°C)	
	Δ T product (°C)	

nt ? C	Process step	Manual mode: Loading (Pre-cooling)	Freezing	Freezing	Freezing	Freezing	1° drying	1° drying	1° drying	2° drying	2°	Manual mode: stooper ing
	Time (hh:mm)		0:15	01:00	0:45	02:00	00:01	01:05	12:00	02:05	02:00	
	Shelf temp. (°C)	20	5	5	-40	-40	-40	25	25	50	50	
	Vacuum (mbar)	off	off	off	off	off	0.15	0.15	0.15	0.15	0.15	750
	Safety pressure (mbar)	off	off	off	off	off	0.26	0.26	0.26	0.26	0.26	
	Δ T shelf (°C)		off	off	off	off	off	off	off	off	off	
	Δ T product (°C)		off	off	off	off	off	off		off	off	
	LyoControl Rx (%)		off	off	off	off	off	off	off	off	off	
	camera interval (min)		15	60	1	5	10	10	10	10	60	



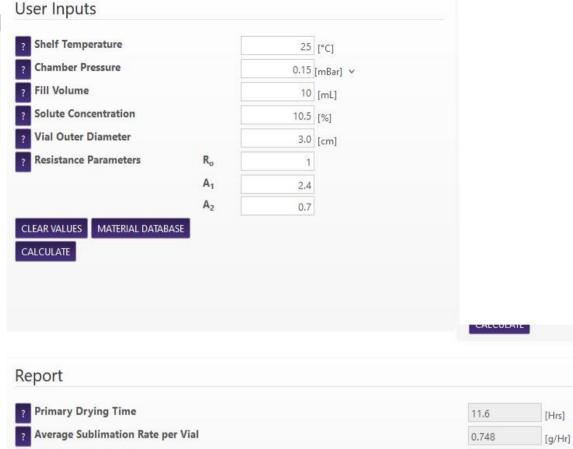
# Aggressive Cycle

Maximum Product Temperature

DETAILED OUTPUT

#### Material Database

	Materials	Ro	A <sub>1</sub>	A <sub>2</sub>
USE	Povidone, 5% (v/v)	1.1	5	0
USE	Sucrose, 5% (w/w) with ice nucleated at -5°C	1	2.4	0.7
USE	Sucrose, 5% (w/w) with ice nucleated at -10°C	1.5	3,4	0.7
USE	Sucrose, 5% (w/w) with ice nucleated at -15°C (note: values were extrapolated)	2.3	5.3	0.7



DOWNLOAD DATA AS CSV

-25.6

[°C]

### Calculated "by hand":

- $T_s = \sim -4^{\circ}C$
- $Pc = ~97 \text{ mTorr} = 129 \mu bar$

